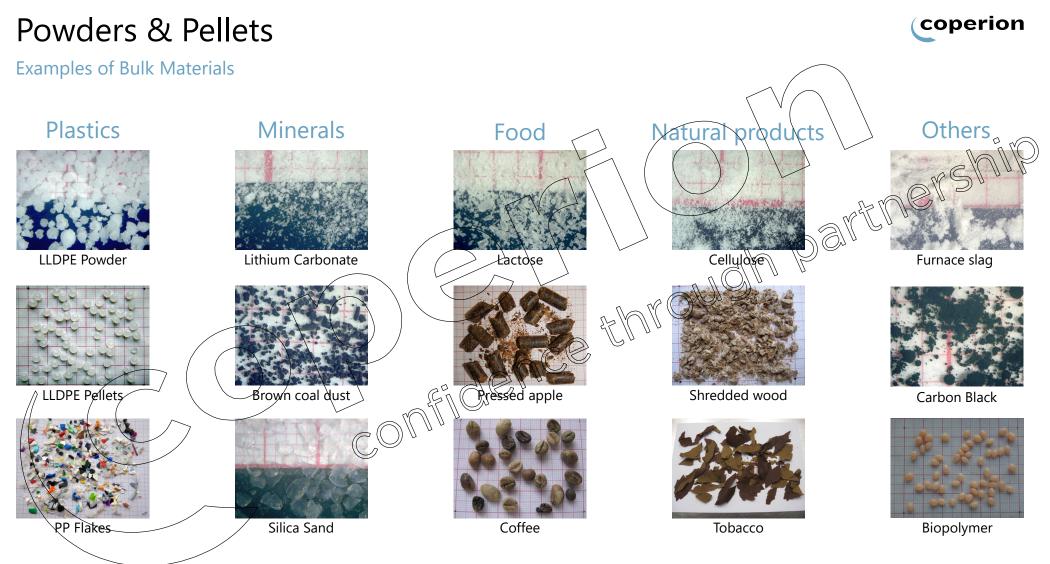
Material Handling – Basic Principle

Christoph Schumacher – General Manager Materials Handling Plants & Systems





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Powders & Pellets coperion Examples in Plastics & Chemicals Powder / Granules / Flakes (from Reaction / Polymerisation) Enership Pellets (under water pelletized /extruded)

Plastics & Chemicals

Characteristics

General bulk solids evaluation

- Accumulating / caking
- Forms wall deposits
- Strength of particles/agglomerates
- Adhesive
- Bridging due to particle shape
 - only when deaerated
 - due to cohesion
- /Free-flowing
- Fluidizable
- Erratic flow
- •\Particle hardness
- Agglomerating

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Typical measured Bulk Solids data

And / Particle Density Bulk Density / Packed Density Particle size / distribution

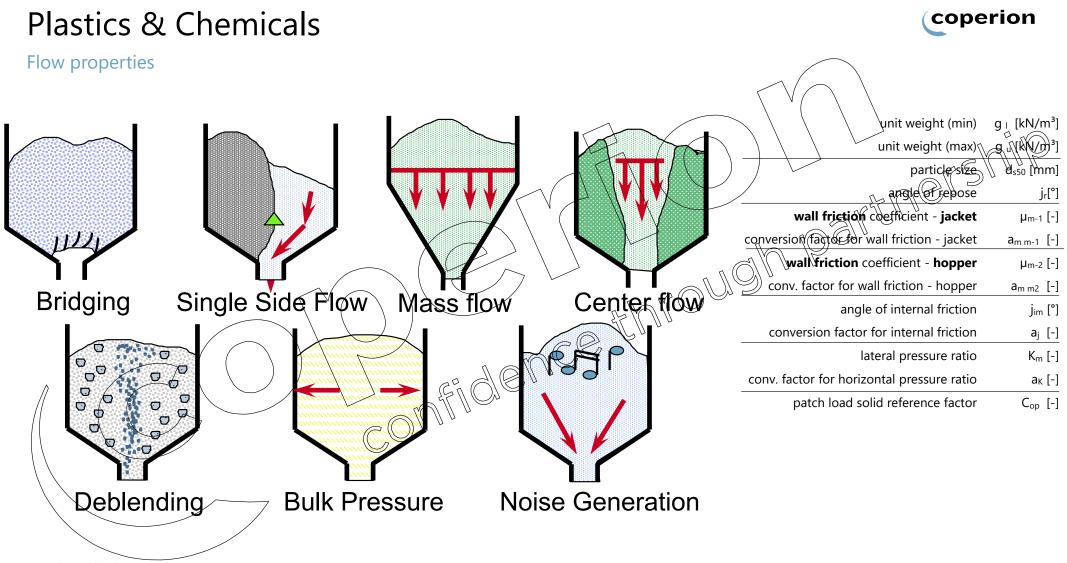
- Product perature 12m
- **Particle Shape**
- Strand / Under water cut
- E-Modulus / Secant Modulus
- MFI



coperion **Plastics & Chemicals Geldart Diagram** Limit of pneumatic conveying Dilute / Strand conveying, A (unstable area) Slug Phase conveying Bulk Density [kg/m³] products Dilute Phase conveying Heavy products Β C without pressure minimum 1000 **S** (Deposits) hre ohesi Fluidizing Standard products products Dilute / Strand conveying, Ŭ С (Dense Phase flow conveying) D **Dilute Phase conveying** D 100+ 0,01 (Coating) 10 0.1 Particle size [mm] nach R. Pan

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coperion **Pneumatic Conveying Basics: Definition and Variables** partnership transport of bulk material with a gas flow in a pipeline confidem diameter capacity volume flow velocity length, height, bends particle properties Conveying phases Depending on the selection of the variables, the bulk material moves in different ways through the pipe → Conveying Phases / Coperion Technology Update 2025 8

Conveying Modes coperion Phase Diagram for <u>Pellets</u> 25 FLUIDLE 1 CONVEYING PRESSURE [Δp] FLUIDLIFT Slug 3 **CONTI-SCHUB** 5 Dilute Phase Dense Rhase Unstable Area FLUID-SPLIT (only coarse powder) 4 Phase 1 TAKT-SCHUB 4 Strand Phase 2 Clean Gas ACU-TAKT ACU-SCHUB TERMINAL VELOCITY OF CONVEYING GAS [v.]

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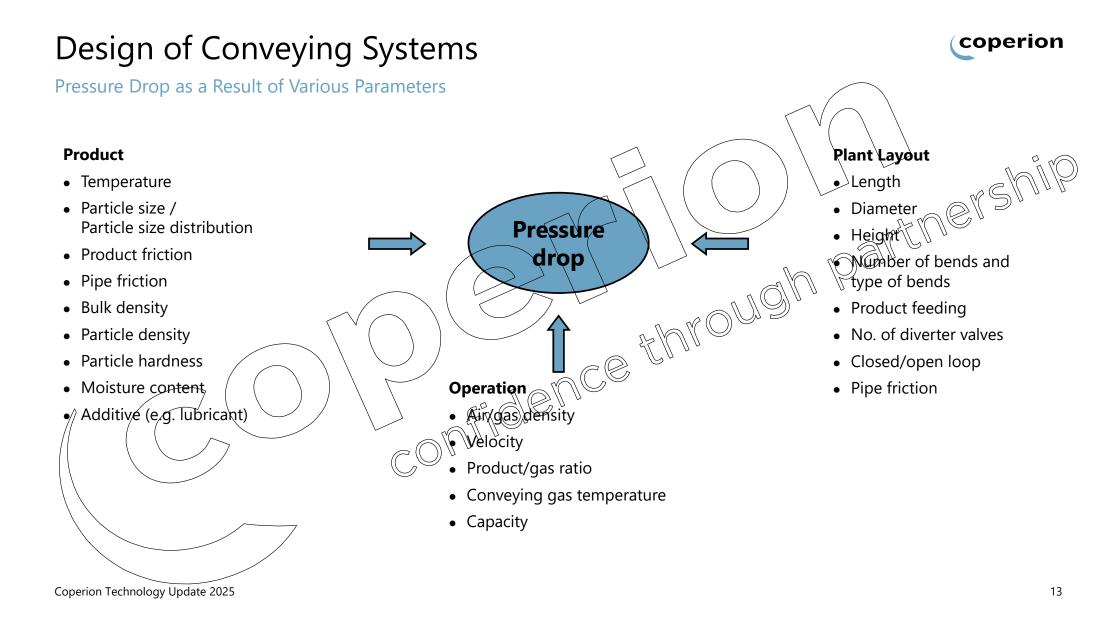
coperion **Conveying Modes** Phase Diagram for Powder Ń CONVEYING PRESSURE [Δp] FLUIDLIFT 2 4 hro Conveying capacity = constant SUPERDENSE 3 Stran Fluid Phase FLUIDSTAT NT Slug Phase 4 DUROSTAT 3 Clean Gas Unstable Area TERMINAL VELOCITY OF CONVEYING GAS [v]

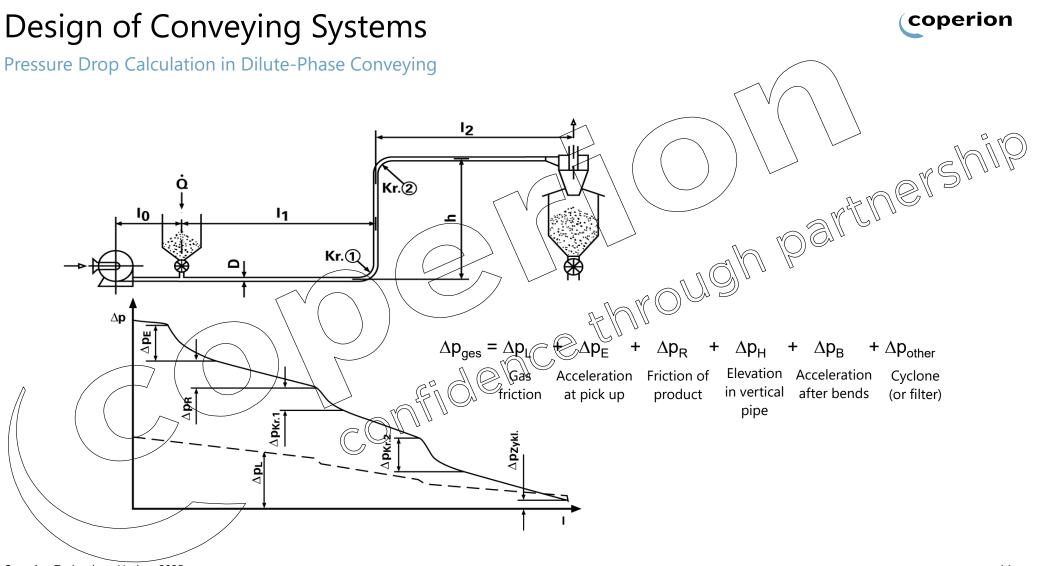
Conveying Modes

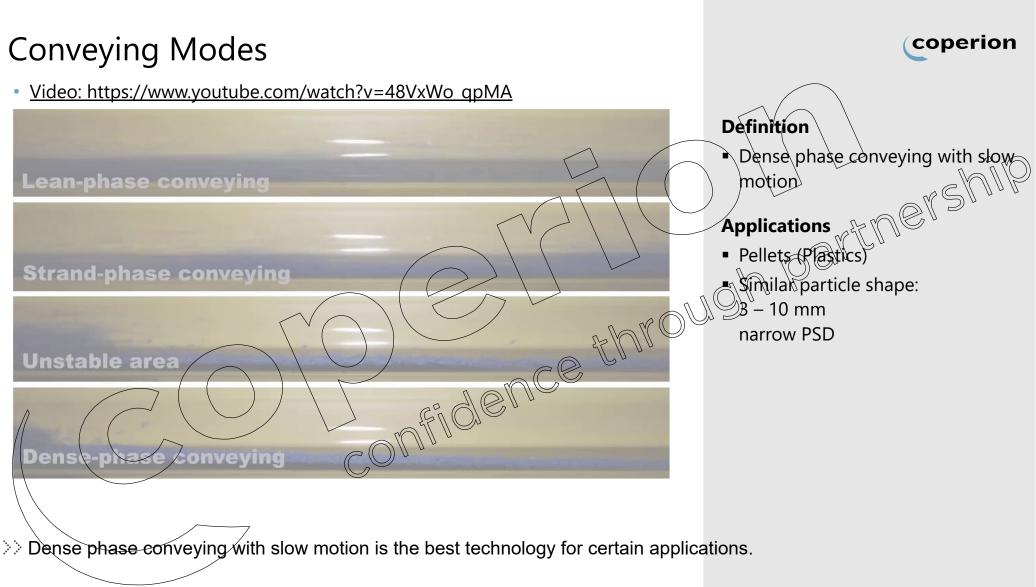
Overview

	Conveying mode	Characterised by	Products	Trade Name	Π
	Dilute-phase (lean phase)	High energy consumption High operational reliability			rsh
	Dense-phase (strand phase)	Low energy consumption Smaller pipe size	Free flowing products (fluff, granules, pellets)		
	Slow motion dense phase (plug phase)	High load ratio Less dust and streamers Low wear	Pellets	CONTI-SCHUB® TAKT- SCHUB®	
	Dense-phase (fluid phase)	Low energy consumption Smaller pipe size	Pluidisable powders	SUPER DENSE®	
	Dense-phase with internal bypass	Self stabilising No obstruction	Powders with average fluidisation properties,finely-grained bulk material	FLUID-STAT®	
- [] -] -	Dense-phase with external bypass (plug phase)	No obstruction Gentle conveying	Non-fluidisable powders, fine to coarse bulk material	FLUID-SPLIT®	

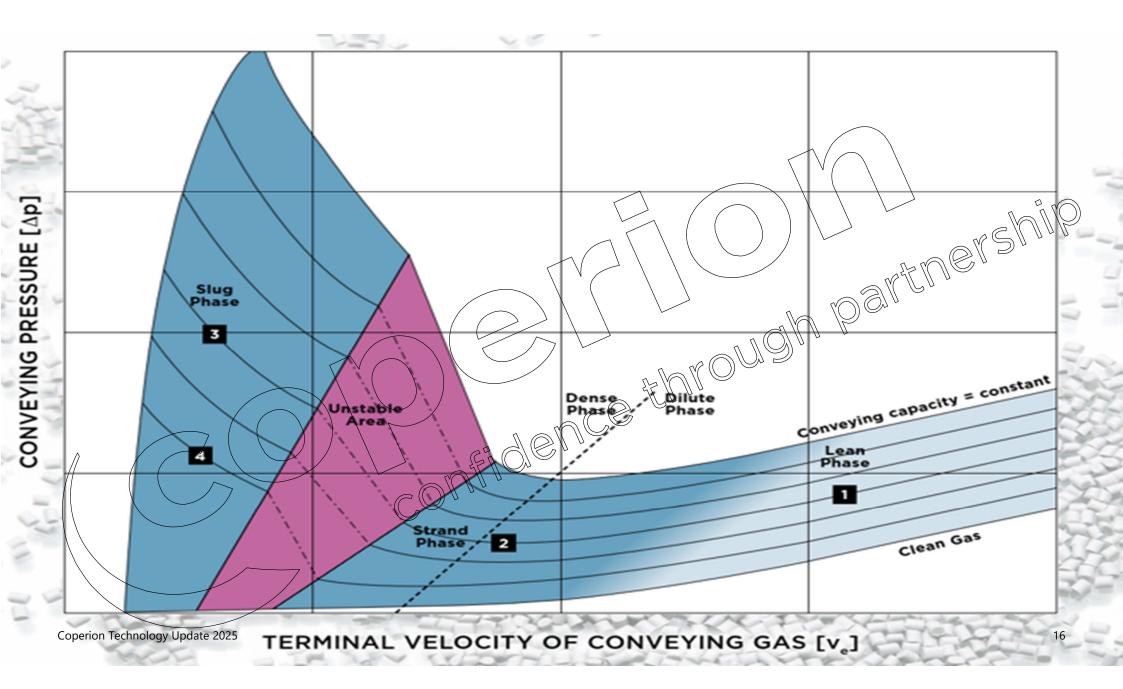




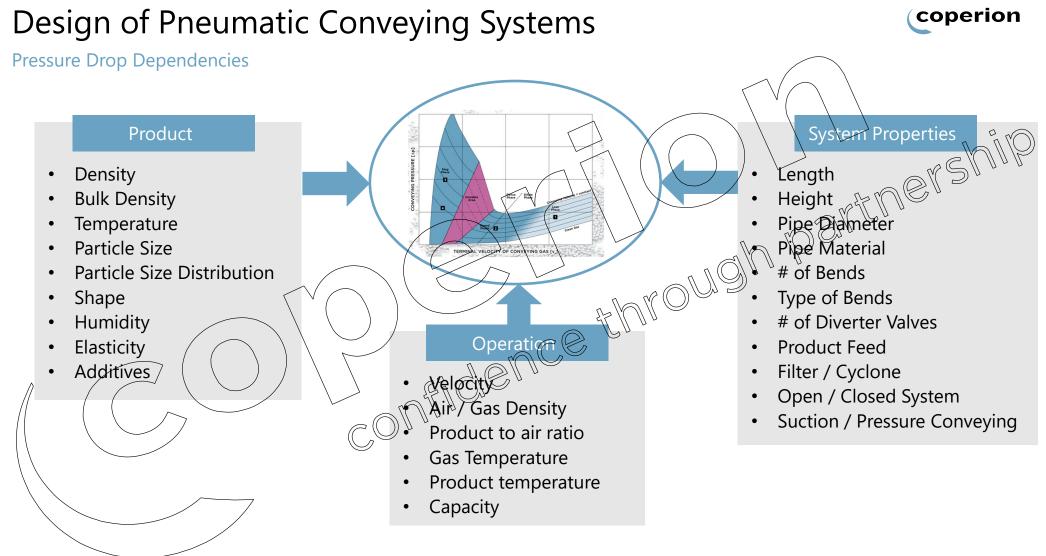




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coperion Design of Pneumatic Conveying Systems Introduction Aım **Design Parameters** • Reliable function with Conveying pressure guaranteed capacity depending on product type and properties, conveying pipe isometric, operating • Minimum impact on conditions, conveying mode, available pressure supply Fidence throug product quality and • Air volume, air velocity creation of fines dust / keep minimum and maximum velocities streamers • Product/Gas-ratio Economical solution (low •//Pipe diameter investment and operating Stepping of the pipe diameter in order to have moderate velocities along the cost) pipe



Conveying Modes Pellet and Coarse Powder Conveying

Lean-Phase Conveying/ FLUIDLEAN[®]

- High gas velocity v = 25 40 m/s
- Low solids loading $\mu = 1-10$
- Low specific pressure drop
- Pressure range $\Delta p = 0.1 1.5$ bar
- Bulk material in suspension flow



Strand Conveying/ FLULDLLFT®

- Gas velocity v = 15 30 m/s
- Greater solids loading $\mu \neq 5 + 25$
- Low specific pressure drop
- Pressure range $\Delta p = 0.5 3.0$ bar

 (\bigcirc)

Bulk material floating, sliding or recumbent bulk strand

FLUIDLIFT ecoblue

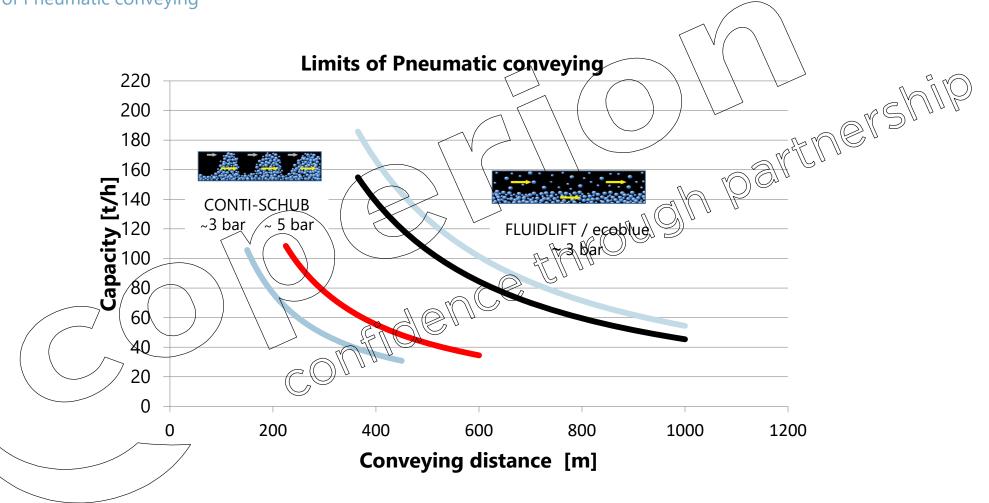
- Enhancement of FLUIDLIFT®
- Stiding strands with reduced friction
- Water injection into conveying air

Slug Conveying / CONTI-SCHUB®

- Low gas velocity v = 10m/s
- High solids loading $\mu = 10 50$
- High pressure drop Pressure range $\Delta p = 0.5 - 6$ bar
- Bulk material concentrated in plugs ("Plug conveying")
- Self-acting formation of the plugs (CONTI-SCHUB[®],
- Artificial plug formation may be necessary (TAKT-SCHUB[®])

Pellet Convey at Throughput

Limits of Pneumatic conveying



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Design of Pneumatic Conveying Systems

Technical Center: Features

- Full size conveying systems (up to DN200) for investigating pneumatic conveying in dilute phase / dense phase including impact forces
- Conveying can be done with different feeding devices
- Full size conveying systems (up to DN100) for conveying of difficult powders (normal piping / FLUIDSTAT / FLUIDSPLIT / flexible rubber pipe)
- Conveying system for suction conveying
- Insulated conveying system to measure temperature influence on conveying pressure
- Rotary valve test station for full size capacity/tests of rotary valves (up to rotor size 800)
- Conveying system (for determination of fines creation in all common pipe materials / surfaces / with different bend types and possibility of variation of temperature
- Complete hydraulic conveying system (DN(TOO)
- Various pellet cleaning devices (UGS / HFS)
- More than 800 evaluated conveying tests
- More than 10.000 analyzed lab product samples \rightarrow High number of data sets for designing pneumatic conveying systems





Thank you very much for your attention.

